PROMOTED HYDROLYSIS OF SOME ORGANOPHOSPHATE ESTERS USING SUPPORTED [Cu(tmen)OH(OH2)]+

Murat ERDEM *

Department of Chemistry, Faculty of Science, Anadolu University, Eskişehir, Turkey

ABSTRACT

In this study, tetramethylethylenediamine copper(II) complex ($Cu(tmen)Cl_2$) was synthesized and natural clay smectite and synthetic Dowex-50WX8 resin containing $Cu(tmen)(OH)(OH_2)^+$ were prepared via ion exchange process in aqueous solution. Dowex- and smectite-supported $Cu(tmen)(OH)(OH_2)^+$ were used as a supported catalyst in the hydrolysis reactions of organophosphate compounds of diethyl-*p*-nitrophenyl phosphate and *p*-nitrophenyl diphenyl phosphate at different pH values. Scanning electron microscope attached with energy dispersive X-ray dedector and surface area analyzer were used for the characterization of the supported catalysts. The efficiency of these supported catalysts was evaluated in accordance with pseudo-first-order and Michaelis-Menten enzyme kinetic models. The amount of copper(II) complex in Dowex-supported catalyst was higher than that of smectite-supported one (1.36 mmol/g and 0.88 mmol/g, respectively) and the higher efficiency was obtained when Dowex-supported catalyst was employed in all of the hydrolysis reactions. 222 and 114-fold increasing in pseudo-first-order rate constants compared to the reactions without supported catalyst were observed for the hydrolysis of diethyl-*p*-nitrophenyl phosphate at pH 8.0 in the presence of Dowex-supported and smectite-supported catalysts.

Keywords: Dowex-50WX8, Smectite, Tetramethylethylenediamine copper(II) complex, Diethyl-*p*-nitrophenyl phosphate, *p*-Nitrophenyl diphenyl phosphate

1. INTRODUCTION

Organophosphate esters have been used as insecticides for many years to protect the crops and animals from harmful effects of insects. Their toxicity and persistence in the environment is causing short and long term health problems in humans. Parallel to insecticide development, appreciation of their potential lethality also led to consideration of their use as chemical warfare agents. Although modern chemical weapons (known as nerve agents) have been used in limited circumstances, large quantities of agents such as sarin, soman and tabun are still stockpiled in a number of countries around the world, and their destruction requires the use of environmentally friendly processes. Both nerve agents and insecticides act as an inhibitor for enzyme acetylcholinesterase which is responsible for regulating the concentration of the neurotransmitter acetylcholine [1-5].

Although the use of organophospahate esters as insecticide or herbicide is important to the agricultural industry, their extensive use can also lead to poisoning due to the exposure of large numbers of people worldwide. Moreover, their accumulation in the environment is a recognized ecological threat with harmful effects on living species [6]. Despite the intense research during the second half of the last century, the detoxification or decontamination of organophosphate esters is still a serious problem. Thus, many researchers have been attracted to develop phosphorolytic decontaminants for the cleavage of organophosphate ester compounds. For this purpose, many detoxification agents such as metal complexes and metallomicelles [7-11], *o*-iodosylcarboxylates and polymer-supported *o*-iodosylcarboxylates [12-16], α-effect nucleophiles [17, 18], biological catalysts [19, 20], substrate imprinted polymers [21, 22] have been developed.

*Corresponding Author: merdem@anadolu.edu.tr

There has been considerable interest in the area of metal-hydroxo nucleophiles and their role in promoting the hydrolysis of organophosphate esters. Metal ions may simultaneously act as nucleophiles by providing a metal-hydroxide to perform an intramolecular attack [23]. The tetramethylethylenediamine copper(II) complex, $[Cu(tmen)(OH)(OH_2)]^+$, was one of the first metal complexes used for the hydrolysis of organophospahates [24]. A drawback of these homogeneous catalyses is the impossibility to recover and recycle the catalyst while the supported catalyst can easily be isolated and recovered by precipitation and filtration. Immobilization of the catalysts on an insoluble matrix can provide a simple solution to this problem. Polymer-supported metals or metal complexes have been widely used heterogeneous catalysts active in the cleavage of phosphoric esters for last years. Hartshorn and coworkers [25] synthesized N-vinylbenzyl-based polymeric supports containing Cu(II)-1,4,7-triazacyclononane complex and examined their catalytic performances towards methyl parathion (MeP) and bis-(4-nitrophenyl) phosphate (BNPP). The hydrolysis rates obtained with their catalysts are among the higher reported for the polymer-supported hydrolysis of MeP and BNPP. In another study, a series of polymer-supported bidentate amine Cu(II) complexes were obtained and hydrolytic decomposition of the nerve agent, sarin, was studied [26]. Styrene- and (meth)acrylate-based linear polymers, poly(vinylbenzyl chloride)- and methacrylate-based macroporous resins, 8-hydroxyquinoline containing methacrylate resins, methacrylate- and acrylate-based hydrogels were selected as support to attach complexes. Bukowski et al. [27] prepared a family of copolymeric hydrogels containing vinylimidazole, acrylamide and *N,N'*-methylenebisacrylamide to bind Cu(II) ions. The hydrolysis activity of obtained Cu(II)-loaded hydrogels towards bis(3-nitrophenyl)phosphate was five orders of magnitude greater than the uncatalyzed reaction. Mersal and Ibrahim [7] investigated the hydrolysis of parathion catalyzed with both Zn(II) and Cu(II) complexes of tris(2-benzylaminoethyl)amine (BzTren) and the kinetic results indicated that Cu(II) complex is more active than Zn(II)-BzTren.

Although the organophosphate hydrolysis promoted by $[Cu(tmen)(OH)(OH_2)]^+$ have been reported, studies on efficiency of smectite- and Dowex 50WX8-supported $[Cu(tmen)(OH)(OH_2)]^+$ are not available in the literature. In this study, supported $Cu(tmen)(OH)(OH_2)^+$ were prepared and used as supported catalysts for the hydrolysis of model compounds diethyl-*p*-nitrophenyl phosphate (paraoxon, PO) and *p*-nitrophenyl diphenyl phosphate (PNPDPP) in basic aqueous solutions. A natural clay smectite (Sm) and cation exchange resin Dowex-50WX8 (Dw) were used as support. The effects of pH and temperature on the efficiency of the supported catalysts were investigated.

2. EXPERIMENTAL

2.1. Materials

Paraoxon, Dowex-50WX8 (Diethenyl-benzene polymer with ethenylbenzene and ethenylethylbenzene, sulfonated), *N,N,N',N'*-tetramethylethylenediamine, TAPS buffer compound, $CuCl_2.2H_2O$, methanol and diethyl ether were purchased from Sigma-Aldrich (USA). PNPDPP was synthesized according to the literature [28].

2.2. Synthesis of Copper(II) Complex of *N,N,N',N'*-Tetramethylethylenediamine

Synthesis of copper complex of *N,N,N',N'*-tetramethylethylenediamine ($Cu(tmen)Cl_2$) was carried out as follows: A solution of *N,N,N',N'*-tetramethylethylenediamine (tmen) was prepared via dissolution of 2.90 g of the ligand in ethanol (80 mL) then a solution of $CuCl_2.2H_2O$ (5.1 g) in methanol (200 mL) was added dropwise with stirring to the solution of tmen. The solution was evaporated to the total volume of 150 mL. After crystallization of the dark blue complex, it was filtered off and recrystallized from methanol-diethyl ether and dried in a vacuum oven at 40°C. $[Cu(tmen)Cl_2]$ was characterized with elemental analysis. Elemental analysis: Calculated for $C_6H_{16}N_2Cl_2Cu$ (FW 250.66): C, 28.75; H, 6.43; N, 11.18. Found: C, 28.54; H, 6.51; N, 11.12. The chemical structure of the complex is given in Figure 1.
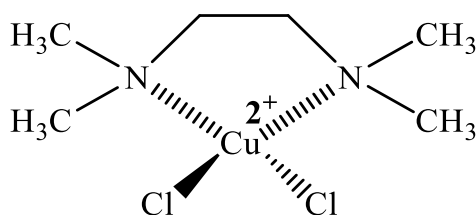
Figure 1. The chemical structure of [Cu(tmen)Cl$_2$]

2.3. Preparation of Supported Catalysts

The supported catalysts were prepared by means of ion exchange process. Before the exchange, Dw was washed with 0.1 M HCl solution to eliminate undesired impurities. Thereafter, Dw was washed several times with double distilled water to remove all the excess acid and chloride anion.

A certain amount of dry support (dried a day at 50 °C in a vacuum oven) was added to the aqueous solution of Cu(tmen)(OH)(OH$_2$)$^+$. After stirring a period of 5 h at room temperature, the solid was filtered and washed with double distilled water several times. Then the solid was dried in a vacuum oven at 50 °C overnight. Elemental analysis was done to determine the amount of the complex per gram of dry solid. Dowex- and smectite-supported Cu(tmen)(OH)(OH$_2$)$^+$ were named as Dw-Cu and Sm-Cu, respectively. Some physical and quantitative characteristics of the supported catalysts are given in Table 1.

Table 1. Some physical and quantitative characteristics of the supports and supported catalysts

Parameters	Dw	Sm	Dw-Cu	Sm-Cu
BET surface area (m^2 g^{-1})	7.08	80.33	12.51	94.60
Micropore area (m^2 g^{-1})[a]	0	8.20	0	41.17
External surface area (m^2 g^{-1})[a]	7.08	72.13	12.51	53.43
Total pore volume (cc g^{-1})[b]	7.20×10^{-3}	9.03×10^{-2}	1.27×10^{-2}	1.56×10^{-1}
Average pore diameter (Å)[c]	20.32	22.47	20.23	32.93
Amount of complex (mmol g^{-1})[d]	-	-	1.36	0.88

[a]Determined by applying *t*-plot method. [b]Determined at P/P^0 = 0.995. [c]Determined by applying BJH (Barrett, Joyner and Halenda) method [d]Calculated from elemental analysis results

2.4. Characterization of Supported Catalysts

Scanning electron microscope attached with energy dispersive X-ray (EDS, EDAX) dedector (SEM, Carl Zeiss Ultra Plus) was used to investigate the surface morphologies and elemental compositions of Dw-Cu and Sm-Cu after gold coating processes. The amount of Cu(tmen)(OH)(OH$_2$)$^+$ bound to Dw and Sm was calculated from the elemental analysis were done using Vario III Elementar element analyzer.

2.5. Kinetic Measurements

In a typical reaction, the supported catalyst (10 mg) was suspended in 4.75 mL of TAPS buffer (pH 9.0) and incubated in a period of 10 min. 0.5 mL of the substrate stock solution in acetonitrile was added to the suspension containing the supported catalyst. At certain times, the suspension was centrifugated and

the absorbance of *p*-nitrophenolate anion (NP) which is the product of hydrolytic reaction of the substrates in the supernatant was determined spectrophotometrically at 400 nm. From the absorbance values of NP, its concentration was determined using an appropriate calibration curve of NP and the kinetics of the hydrolysis reactions were determined. Initial reaction rates (IRR) of the reactions were determined from NP concentration versus time (Figure 2, inset).
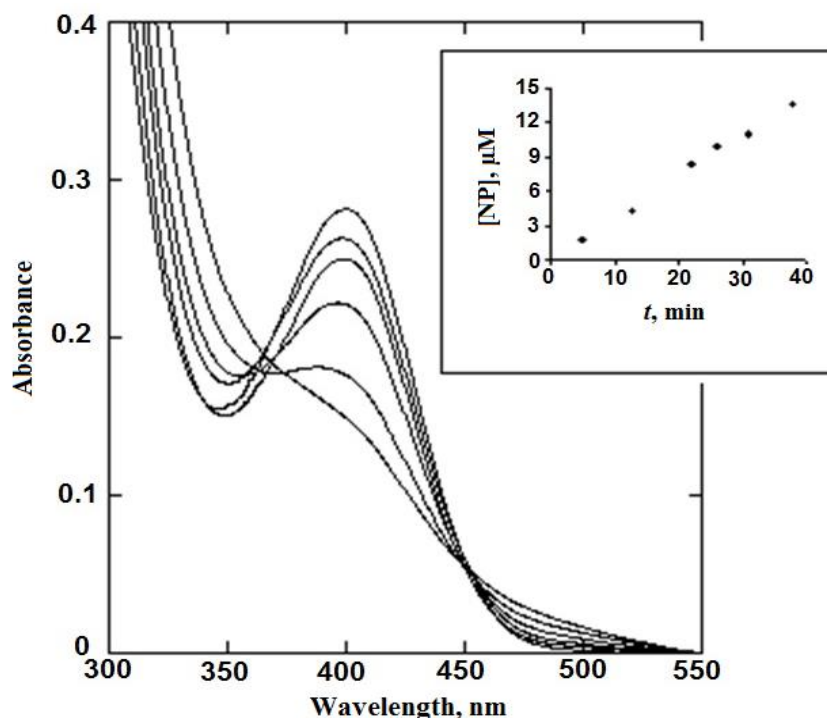

Figure 2. Increasing of NP absorbance with time for the hydrolysis of PO promoted by Dw-Cu and time dependence of the concentration of NP released from hydrolysis reaction (Inset). Reaction conditions: $[Cu^{2+}] = 1.36$ mM, $[PO] = 5 \times 10^{-4}$ M, $[TAPS] = 5$ mM, pH = 9.0, 25°C

3. RESULTS AND DISCUSSION

3.1. Characterization of Supported Catalysts

SEM images and EDS spectra of the supported catalysts are shown in Figure 3a-d. The images revealed that Sm-Cu had rough and porous surface character, while spherical morphology was observed for Dw-Cu. The presence of Cu in both supported catalyst was clearly seen from EDS results. Moreover, the amount of $Cu(tmen)(OH)(OH_2)^+$ in Dw-Cu and Sm-Cu was calculated from the elemental analysis results as 0.88 mmol/g and 1.36 mmol/g, respectively (see Table 1).
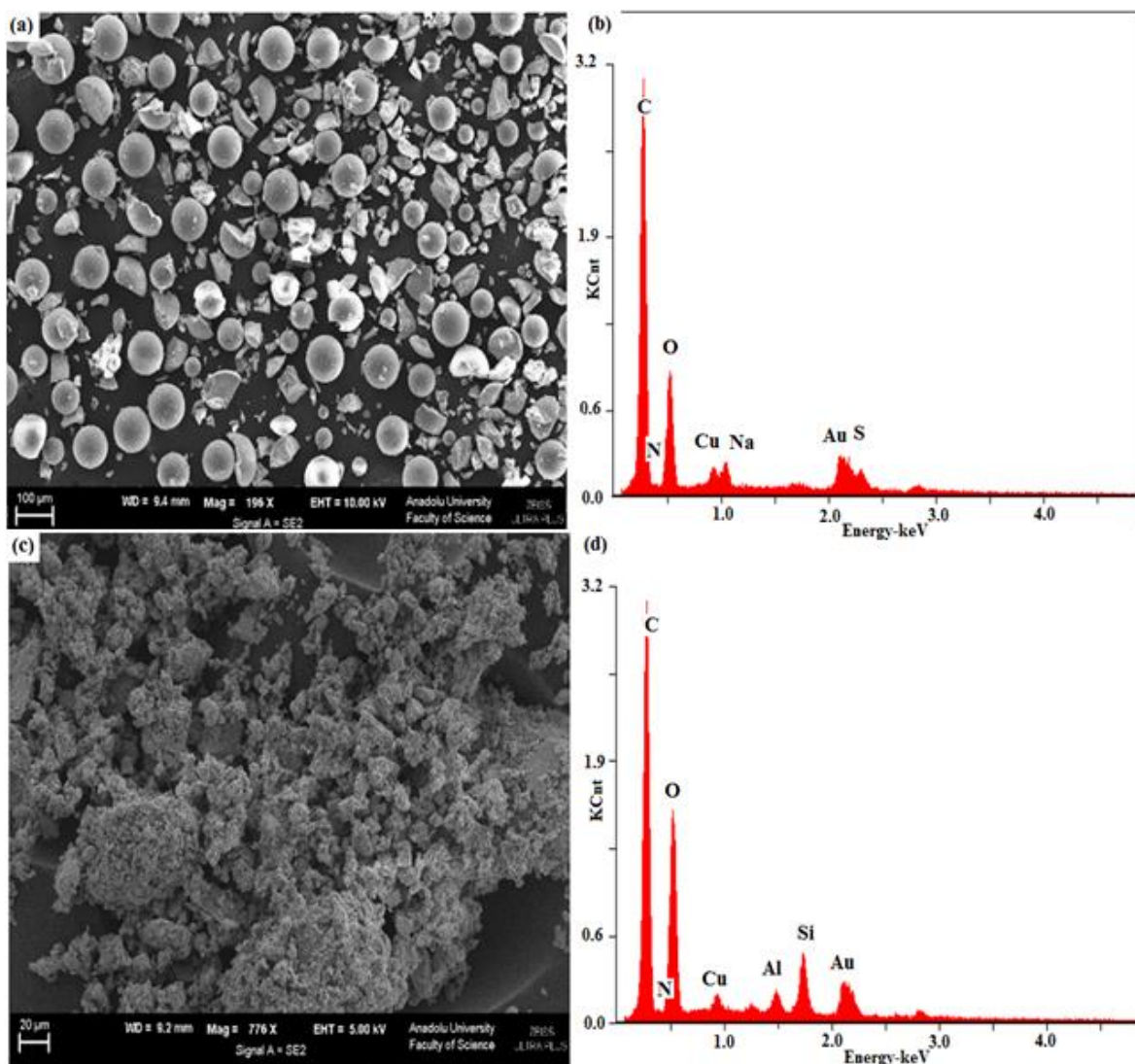
Figure 3. SEM images of (a) Dw-Cu and (c) Sm-Cu and EDS spectra of (b) Dw-Cu and (d) Sm-Cu

3.2. Kinetics of PO and PNPDPP Hydrolysis

To evaluate the efficiency of Dw-Cu and Sm-Cu for the hydrolysis of PO and PNPDPP, kinetic investigations were carried out at pH 7.0, 8.0, 9.0 and 9.5 at 25°C. In previous works, authors have used pseudo-first-order kinetic model to evaluate the time dependency of organophosphate hydrolysis catalyzed by metal complexes and their polymer supported derivatives [27, 29, 30]. The rate equation of the hydrolysis of organophosphates such as PNPDPP and PO catalyzed by metal complexes in basic conditions can be given as:

$$Rate = \frac{-d[Substrate]}{dt} \tag{1}$$

$$Rate = k_2[Cu(tmen)(OH)(OH_2)^+][Substrate] + k_{OH}[OH^-][Substate] \tag{2}$$

In this rate equation, the terms $k_2[Cu(tmen)(OH)(OH_2)^+][Substrate]$ and $k_{OH}[OH^-][Substrate]$ represent the contributions of metal complex catalyzed and OH^- catalyzed reactions on the total hydrolysis rate of substrate, respectively. At constant $Cu(tmen)(OH)(OH_2)^+$ and OH^- concentrations, these values become

constant, then the rate of hydrolysis becomes linearly dependent only on the concentration of substrate (Eq. (3)).

$$Rate = (k_2[Cu(tmen)(OH)(OH_2)^+] + k_{OH}[OH^-][Substrate]) = k_{obs}[Substrate] \quad (3)$$

Under these conditions, the hydrolysis of substrates are first-order reaction. The integrated form of Eq. (3) is given below (Eq. (4)).

$$ln\left(\frac{[Substrate]}{[Substrate]_0}\right) = -k_{obs}t \quad (4)$$

The plot of ln([Substrate]/[Substrate]$_0$) against t yields a straight line whose slope equals $-k_{obs}$.

The pseudo-first-order kinetic plots for PO hydrolysis over a pH range of 7.0-9.5 are shown in Figure 4 and k_{obs} values for PO and PNPDPP hydrolysis are tabulated in Table 2. For both substrates, the values of k_{obs} increased with increasing pH and then decreased with its further increasing. The highest k_{obs} values were obtained with Dw-Cu at pH 9.0 for both substrate. When compared k_{rel} values, the best efficiency in the hydrolysis of the substrates was achieved at pH 8.0. k_{obs} values obtained at pH 8.0 with Dw-Cu were $2.19×10^{-4}$ min^{-1} for PO and $2.63×10^{-3}$ min^{-1} for PNPDPP.
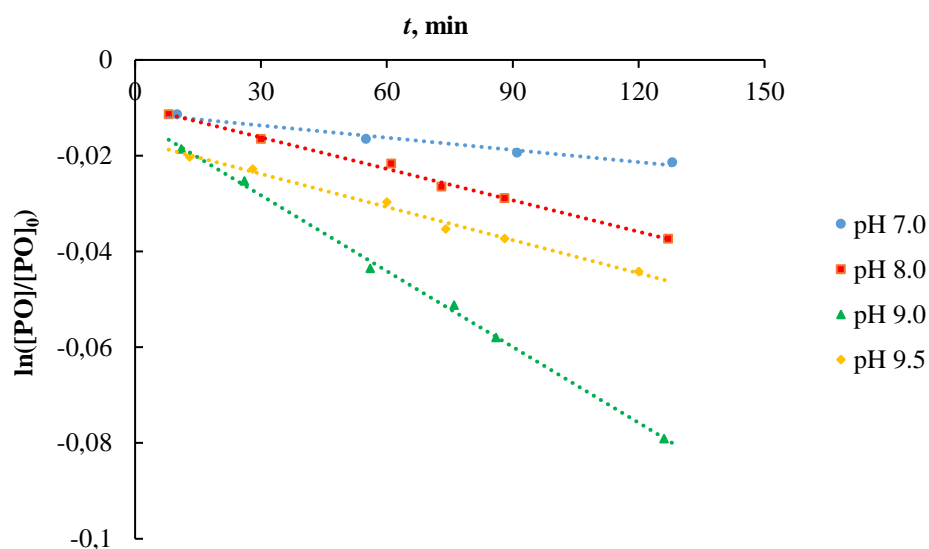

Figure 4. Plots of pseudo-first-order kinetics of hydrolysis of PO with 10 mg of Dw-Cu at pH 7.0, 8.0, 9.0 and 9.5. Reaction conditions: [Cu^{2+}] = 1.36 mM, [PO] = $5×10^{-4}$ M, [TAPS] = 5 mM, 25 °C

Table 2. Pseudo-first-order rate constants for the hydrolysis of PO and PNPDPP at various pH values

pH	Supported catalyst[a, b]	PO		PNPDPP	
		k_{obs} (min^{-1})	k_{rel}[c]	k_{obs} (min^{-1})	k_{rel}[c]
7.0	None	4.12×10^{-7}	1	1.86×10^{-6}	1
	Dw	6.36×10^{-7}	1.5	2.37×10^{-6}	1.3
	Sm	4.75×10^{-7}	1.2	2.22×10^{-6}	1.2
	Dw-Cu	7.79×10^{-5}	189	3.26×10^{-4}	175
	Sm-Cu	4.88×10^{-5}	118	1.08×10^{-4}	58
8.0	None	9.86×10^{-7}	1	9.19×10^{-6}	1
	Dw	9.98×10^{-7}	~1	9.27×10^{-6}	~1
	Sm	9.92×10^{-7}	~1	9.26×10^{-6}	~1
	Dw-Cu	2.19×10^{-4}	222	2.63×10^{-3}	286
	Sm-Cu	1.22×10^{-4}	114	8.87×10^{-4}	97
9.0	None	3.11×10^{-6}	1	4.78×10^{-5}	1
	Dw	3.41×10^{-6}	1.1	5.74×10^{-5}	1.2
	Sm	3.23×10^{-6}	~1	4.89×10^{-5}	1.1
	Dw-Cu	5.28×10^{-4}	170	8.98×10^{-3}	188
	Sm-Cu	2.18×10^{-4}	70	2.21×10^{-3}	46
9.5	None	3.09×10^{-6}	1	2.02×10^{-5}	1
	Dw	3.40×10^{-6}	1.1	2.65×10^{-5}	1.3
	Sm	3.37×10^{-6}	1.1	2.37×10^{-5}	1.2
	Dw-Cu	2.31×10^{-4}	74	1.76×10^{-3}	87
	Sm-Cu	1.39×10^{-4}	45	9.43×10^{-4}	47

[a]Reaction conditions for Dw-Cu and Sm-Cu promoted reactions: [Cu^{2+}] = 1.36 mM for Dw-Cu and 0.88 mM for Sm-Cu, [PO] or [PNPDPP] = 5×10^{-4} M, [TAPS] = 5 mM, 25°C. [b]Potentiometric study was demonstrated that [Cu(tmen)Cl$_2$] complex in aqueous media gives the hydroxoaqua complex Cu(tmen)(OH)(OH$_2$)$^+$ [7]. [c]$k_{rel}=k_{obs}$ of promoted reaction/k_{obs} of the reaction without supported catalyst.

3.4. Michaelis-Menten Kinetics of the Supported Catalysts

Saturation kinetics for the hydrolysis of the substrates with Dw-Cu and Sm-Cu was observed. The effect of PO concentration on the initial rate for the hydrolysis of PO by the supported catalysts at pH 9 and 25°C is shown in Figure 5. The non-linear curves revealed that reactions might follow Michaelis-Menten kinetics and the kinetic parameters for PO hydrolysis, K_M and IRR_{max} were determined from the Lineweaver-Burk plot (Figure 5, related equation is Eq. 5).

$$\frac{1}{IRR} = \frac{K_M}{IRR_{max}}\frac{1}{[S]} + \frac{1}{IRR_{max}} \tag{5}$$

In this equation, IRR_{max} is the maximum reaction rate and K_M is Michaelis constant which reflects the affinity of the supported catalyst towards the substrate. The lower K_M value corresponds the higher affinity. k_{cat} which is another important kinetic parameter was calculated by dividing IRR_{max} by the Cu(II) concentration. For PO hydrolysis with Dw-Cu, IRR_{max}, K_M and k_{cat} were found to be 1.20×10^{-6} M min^{-1}, 2.19 mM and 8.85×10^{-4} min^{-1}, respectively. While for Sm-Cu, the corresponding values were 4.05×10^{-7} M min^{-1}, 6.64 mM and 4.60×10^{-4} min^{-1}. These parameters were also obtained for the hydrolysis of PNPDPP with same supported catalysts and all of them are summarized in Table 3.
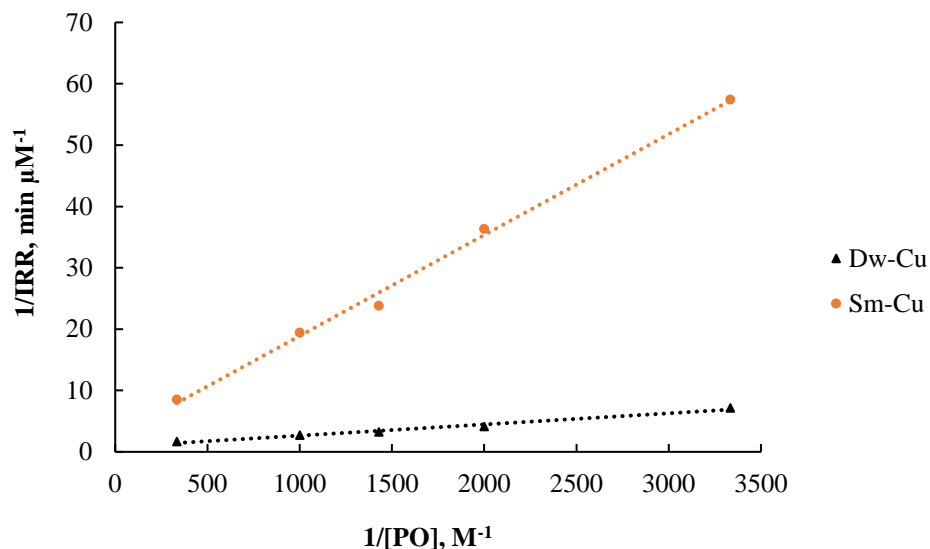
Figure 5. Lineweaver-Burk plots for substrates promoted by Dw-Cu and Sm-Cu. Reaction conditions: $[Cu^{2+}] = 1.36$ mM for Dw-Cu and 0.88 mM for Sm-Cu, [Substrate] = 0.3-3.0 mM, [TAPS] = 5 mM, pH = 9.0, 25°C

Table 3. Michaelis-Menten kinetic parameters for the hydrolysis of PO and PNPDPP at pH 9.0[a]

Substrate	Supported catalyst	IRR_{max}, M min^{-1}	K_m, mM	k_{cat}[b], min^{-1}
PO	Dw-Cu	1.20×10^{-6}	2.19	8.85×10^{-4}
PO	Sm-Cu	4.05×10^{-7}	6.64	4.60×10^{-4}
PNPDPP	Dw-Cu	27.86×10^{-6}	1.11	2.05×10^{-2}
PNPDPP	Sm-Cu	10.79×10^{-6}	1.46	1.23×10^{-2}

[a]Reaction conditions: See Fig. 5 footnotes.[b]$k_{cat} = IRR_{max}/[Cu^{2+}]$

3.5. Effect of Temperature on the Hydrolysis

It is well known that the temperature is one of the most important factor to affect the reaction rate. In this study, some experiments were carried out for the temperature range from 25°C to 65°C to investigate the effect of temperature on the hydrolysis of PO and PNPDPP. Pseudo-first-order kinetic plots of substrates at different temperatures are given in Figure 6. As expected, k_{obs} values for the hydrolysis of both substrate were increased by increasing the temperature. The activation energy of the reaction (E_a) was also calculated from each of these constants at different temperature values. The plots of lnk_{obs} vs. 1/T were drawn (Figure 7) using Arrhenius equation to determine E_a.
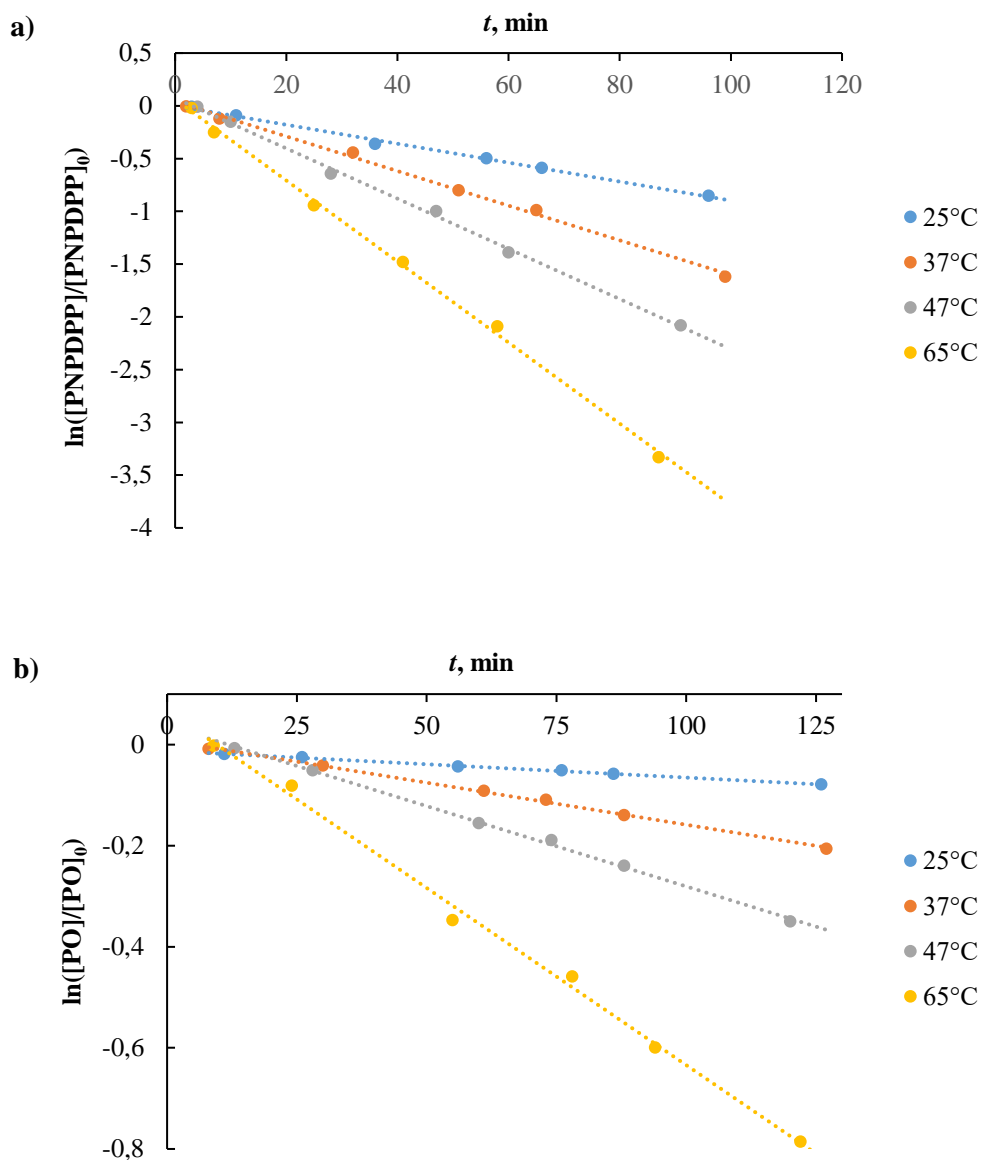
Figure 6. Plots of pseudo-first-order kinetics of a) PNPDPP and b) PO hydrolysis with 10 mg of Dw-Cu at various temperatures. Reaction conditions: pH= 9.0, $[Cu^{2+}]$ = 1.36 mM, [substrate] = 5×10^{-4} M, [TAPS] = 5 mM

As we seen in Table 4, E_a values of the hydrolysis of PO using Dw-Cu and Sm-Cu were found to be 54.6 kJ mol^{-1} and 61.8 kJ mol^{-1}, respectively.

Table 4. The rate constants and E_a values for hydrolysis of substrates at different temperatures[a]

Substrate	Supported catalyst	T, °C	k_{obs}, min^{-1}	E_a, kJ mol^{-1}
PNPDPP	Dw-Cu	25	8.98×10^{-3}	30.8
		37	1.64×10^{-2}	
		47	2.38×10^{-2}	
		65	3.84×10^{-2}	
	Sm-Cu	25	2.21×10^{-3}	35.9
		37	2.65×10^{-3}	
		47	4.91×10^{-3}	
		65	1.10×10^{-2}	
PO	Dw-Cu	25	5.28×10^{-4}	54.6
		37	1.66×10^{-3}	
		47	3.18×10^{-3}	
		65	7.01×10^{-3}	
	Sm-Cu	25	2.18×10^{-4}	61.8
		37	6.82×10^{-4}	
		47	1.50×10^{-3}	
		65	3.85×10^{-3}	

[a]Reaction conditions: $[Cu^{2+}]$ = 1.36 mM for Dw-Cu and 0.88 mM for Sm-Cu, [substrate] = 5.0×10^{-4} M, [TAPS] = 5 mM, pH 9.0
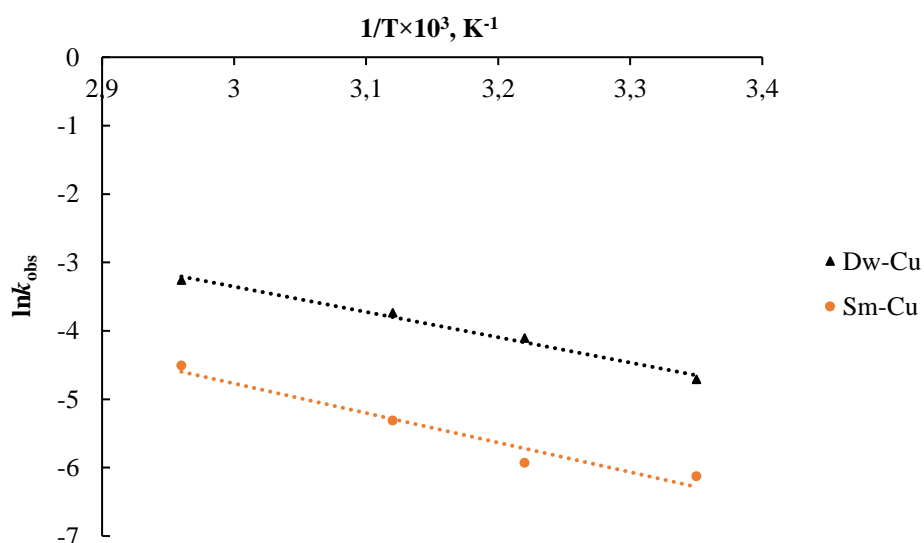

Figure 7. Arrhenius plots for E_a calculations of PNPDPP hydrolysis

4. CONCLUSIONS

The present investigation was aimed to the determination of the efficiency of smectite- and Dowex-supported Cu(tmen)(OH)(OH$_2$)$^+$ for the cleavage of PO and PNPDPP. These systems are very efficient to promote phosphate hydrolysis. The results indicated that both supported catalyst showed a significant rate enhancement and Dw-Cu was found to be more effective than Sm-Cu for the hydrolysis of the substrates. The following conclusions can also be suggested:

✓ As expected, k_{obs} values for the hydrolysis of both substrate were increased by using supported catalyst due to decreasing the activation energy of the reactions.

✓ The efficiency of the supported catalysts are strongly affected by pH. Dw-Cu and Sm-Cu displayed a 222- and 114-fold rate enhancement, respectively, relative to reactions without supported catalyst at pH 8.0.

✓ Although the BET surface area of Sm-Cu 94.60 (m^2 g^{-1}) was higher than that of Dw-Cu (12.51 m^2 g^{-1}) (Table 1), Dw-Cu showed higher efficiency for the hydrolysis of substrates at all kinetic experiments. These findings could be attributed to a higher complex bounding capacity of Dw-Cu which is 1.36 mmol per gram of the support while 0.88 mmol is for Sm-Cu.

✓ Detailed kinetic studies of the hydrolysis reactions were evaluated using Michaelis-Menten plots. It was seen that k_{cat}/K_m values of the supported catalysts towards PNPDPP was higher than that of PO. Also, Dw-Cu was more efficient for the hydrolysis of PO compared to Sm-Cu by a factor of 5.8. Similarly, for PNPDPP hydrolysis this value was determined as 2.2.

✓ It was clearly seen that the efficiency of supported catalysts increases, when the activation energy of the hydrolysis reactions decreases.

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